# Effect of sulfur dioxide concentration on cell performance and sulfur dioxide crossover

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The sulfur dioxide gas is the pollutant gas released in various industrial processes. For example, in the copper refinery process,  $SO_2$  gas is produced to reduce copper sulfide into copper. Most of  $SO_2$  gas produced in the refinery process was converted into sulfuric acid by reaction 1 and 2.

$2 \operatorname{SO}_2 + \operatorname{O}_2 \rightarrow 2 \operatorname{SO}_3$	(1)
$SO_3 + H_2O \rightarrow H_2SO_4$	(2)

To make sulfuric acid and hydrogen simultaneously by using industrial  $SO_2$  off-gas, the  $SO_2$  electrolysis process was proposed. Westinghouse Corporation developed the Hydrid-Sulfur (HyS) process to make hydrogen using sulfur dioxide and electrolyzer [1,2]. The electrochemical reaction has two reactions which are anodic and cathodic reaction.

$SO_2 + 2H_2O \rightarrow H_2SO_4 + 2H_7 + 2e^-$	(3)
$2H+2e^{-} \rightarrow H_2$	(4)

The overall HyS process converts water into hydrogen and oxygen by consuming energy. The first proposed process of Westinghouse used the sulfur dioxide dissolved in sulfuric acid. But, this process has significant diffusion resistance for sulfur dioxide. Therefore, Staser proposed a process that gaseous sulfur dioxide used as a feed [3]. After that, USC (University of South Carolina) studied on water and sulfur dioxide transport in the cell [4,5].

Based on the HyS process, the simultaneous sulfuric acid and hydrogen production process was proposed in the metal refinery process. However, most of  $SO_2$  off-gas in the refinery process contains the air mixed  $SO_2$  because of oxidation process. If without separating air in off-gas, this mixed gas results in overpotential at the  $SO_2$  electrolyzer and it will make more energy consumption. Some processes may be needed to separate the air in the off-gas and economical consideration may be needed.

The electrochemical oxidation studies about HyS process were performed, but the mixed gas effect in the electrolysis reaction was not reported. The objective of this study is to find out the effect of mixed  $SO_2$  gas on the electrochemical cell performance.

Fig. 1 shows the cell voltage difference against SO<sub>2</sub> gas concentration at 0.1 A/cm<sup>2</sup>. While the cell voltage increase based on Nernst equation was 25mV, the cell voltage difference was 85 mV between 20% and 100% SO<sub>2</sub> gas concentration. The reason of difference between experimental and theoretical data might be the increase of mass transport resistance due to mixed N<sub>2</sub> gas.



Fig. 1. Galvanodynamic polarization curves measured from the electrolyzer cell with various  $SO_2$  gas concentrations at 90 °C.

Fig. 2 shows the crossover current density with  $SO_2$  concentration change. The crossover current density was sharply decreased with time by about 50 seconds and then it kept stable within 600 seconds in the range of all  $SO_2$  concentration. The crossover  $SO_2$  was reduced with the change of  $SO_2$  concentration. In this experiment, the proton which was produced on the water side was transported to  $SO_2$  gas side and made hydrogen. The proton transport makes the phenomena of the electroosmotic drag of water. However, the current density of this experiment was so small that the water transport and the  $SO_2$  crossover reduction by electro-osmotic drag were negligible.



Fig. 2. Plot of current density against elapsed time measured from the electrolyzer cell with various  $SO_2$  gas concentrations.

## References

[1] Lu PW, Garcia ER, Ammon RL, J. Appl. Electrochem., **11** (1981) 347.

[2] Lu PW, Ammon RL, J. Electrochem. Soc., **127** (1980) 2610.

[3] John Staser,\* Ramaraja P. Ramasamy,\* Premkumar Sivasubramanian, John W. Weidner, Electrochemical and Solid-State Letters, **10** (2007) E17.

[4] John A. Staser\* and John W. Weidner, J. Electrochem. Soc., **156** (2009) B16-B21.

[5] P. Sivasubramaniana, R. P. Ramasamya, F. J. Freireb, C. E. Hollanda, J. W. Weidner, Int.J. Hydrogen Energy **32** (2007) 463.